


# Why Amine Systems Fail

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Senior Staff Engineer  
Amine Experts Inc.



## Webinar Part Two Gas Processing Focus

 **amine eXperts**


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# Happy New Year!

Welcome to the January 28, 2021 Webinar

Overview of Amine-Based Gas Sweetening  
Part 2

*Mike Sheilan, P.Eng*



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## Introduction

- GPAC is a non-profit organization formed to promote the interaction and exchange of ideas and technology to those involved in the hydrocarbon processing industry.
- GPAC has many exciting things planned for 2021 including 12 technical webinars
- GPAC has operated in Alberta since 1959 because of the support of our membership and generous sponsors. A big thank you to:



### Gold Sponsors



### Silver Sponsors





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## UPCOMING EVENTS

### TECHNICAL WEBINARS



#### 4 Part Hydrogen Series

\$40 for Members \$50 for Non-Members

**PART 1: Hydrogen and the Net-Zero Emission Challenge**  
Presented By: Dr. David Layzell  
February 11<sup>th</sup> | 11:30-12:30pm

**PART 2: The Techno-Economics of Hydrogen as a Fuel**  
Presented By: Dr. David Layzell  
February 19<sup>th</sup> | 11:30-12:30pm

**PART 3: Building a Hydrogen Economy - The Greater Edmonton Region Hydrogen Node**  
Presented By: Dr. David Layzell  
February 25<sup>th</sup> | 11:30-12:30pm

**PART 4: Transportation and Storage Solutions of Hydrogen**  
Presented By: Brian Hall and Andy Jacobson  
March 4<sup>th</sup> | 11:30-1:00pm

Follow us on LinkedIn to stay up to date with GPAC 

### SOCIAL EVENTS

Dates subject to change based on Federal and/or Provincial Health guidelines surrounding Covid-19



**Clay Shooting**  
May 14



**Stampede Lunch**  
July 12



**Classic Golf Tournament**  
September 9

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# WHY AMINE SYSTEMS FAIL!


MIKE SHEILAN, BEN SPOONER,  
PHILIP LE GRANGE



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Mike Sheilan



- 40 years in the industry
- 19 years at Brenntag/Travis Chemicals
  - Technical Service Manager, Dow Chemical support in Canada
  - first supply company to provide engineering technical support to Canadian Oil & Gas Industry
- 21 years at Amine Experts Inc.
  - Senior Staff Engineer – troubleshooting, training, etc.
- Senior Advisor LRGCC at University of Oklahoma
- Published author and Conference Presenter
- Member GPAC, APEGA and NACE

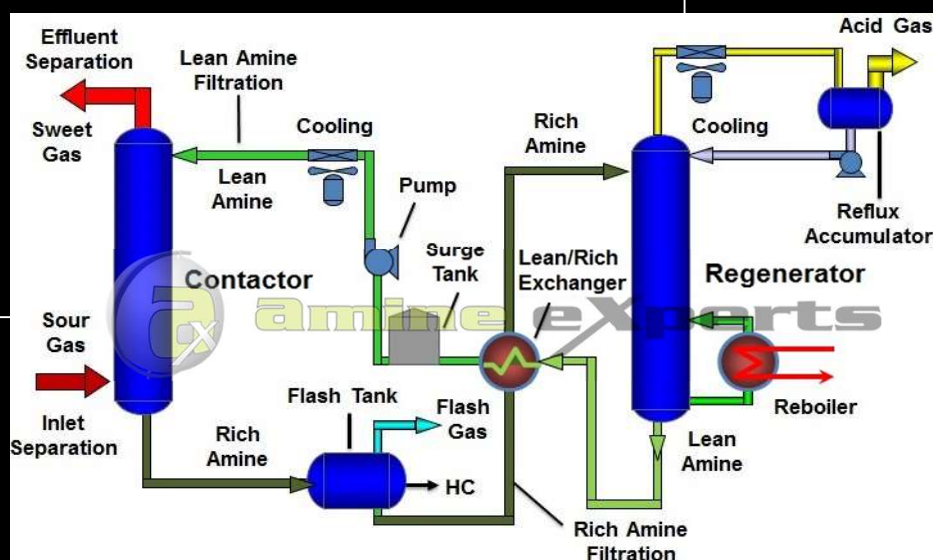
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- Headquartered in Calgary, Alberta
- over 3000 projects in over 60 countries
  - 285 Amine and Sulphur projects in 2019
- senior staff has over 350 years combined experience
- employees have authored more than 70 papers
- provide technical support to every major oil and gas company in the world
- provide technical support to all major process licensors


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## AMINE SYSTEM FLOWSHEET REVIEW




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# INTRODUCTION




Amine Treating is widely used to remove H<sub>2</sub>S & CO<sub>2</sub> from hydrocarbon streams



Maximizing amine unit on-stream time and minimizing process upsets is challenging



A large body of industry knowledge exists, BUT knowing how to apply this at a plant can be daunting (60+ potential root causes of failures)




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# AMINE FAILURES DATABASE

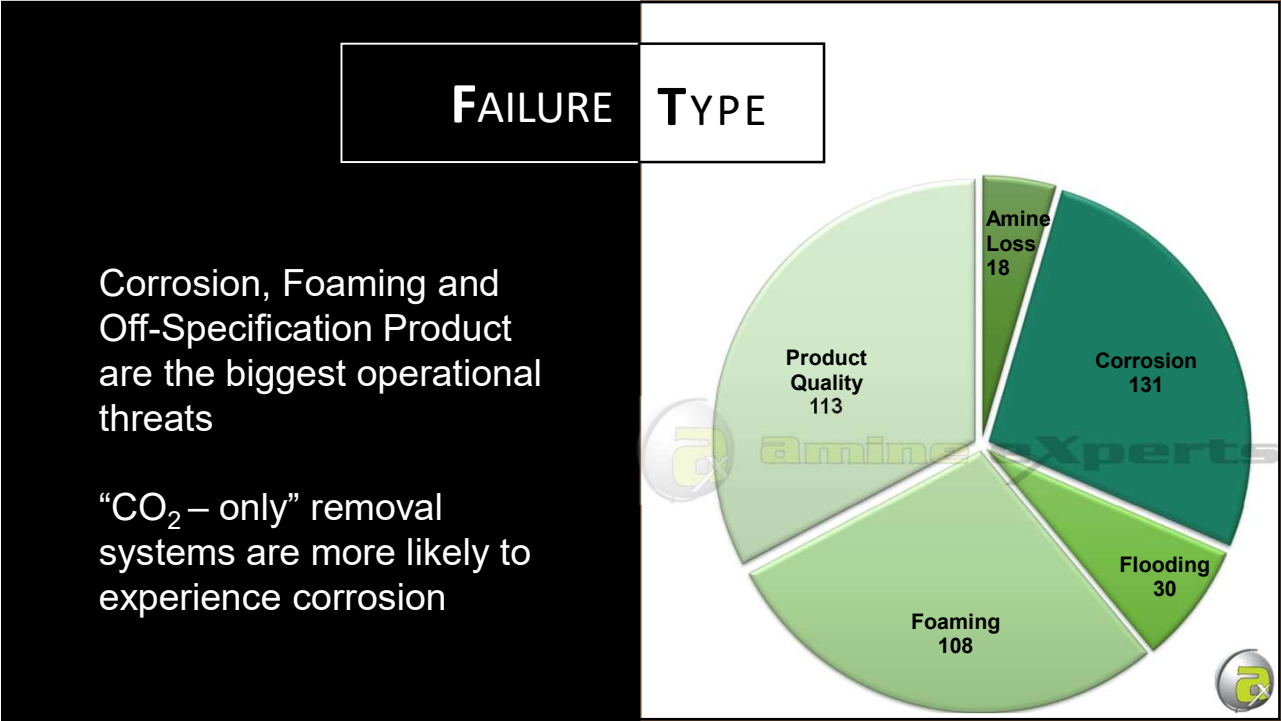
400 incidents of system failure were analyzed

Failure costs ranged from \$100,000 to \$250,000,000 and typically required external assistance to solve

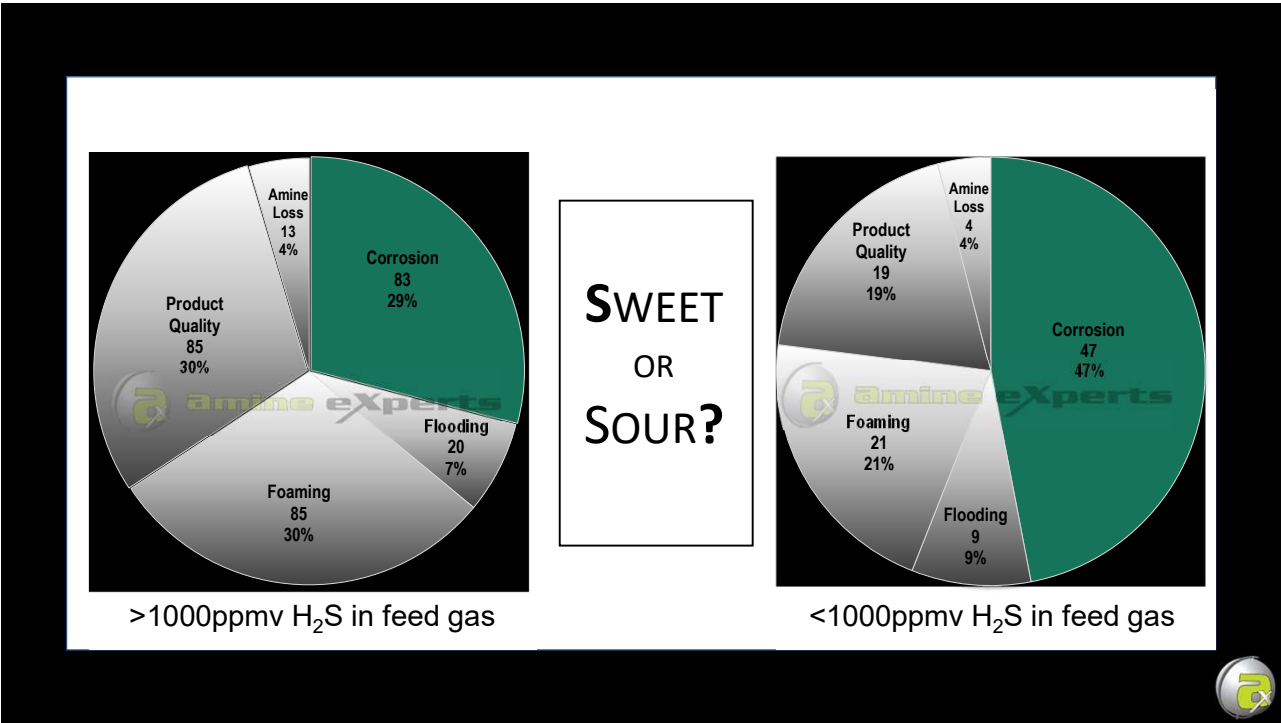
297 cases from Amine Experts site consulting and 103 from literature; most incidents post 1999



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## MEETING SPECIFICATION

CAN YOU AFFORD TO FLARE IF YOU ARE OFF-SPEC?



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## MEETING H<sub>2</sub>S SPECIFICATION

4-16 PPMV

The three factors that most affect treated gas H<sub>2</sub>S content:

- lean amine loading (the lower the better)
- lean amine temperature (the lower the better)
- adequate contact between the amine and gas (H<sub>2</sub>S absorption is *gas-phase dependent*, and *equilibrium limited*)



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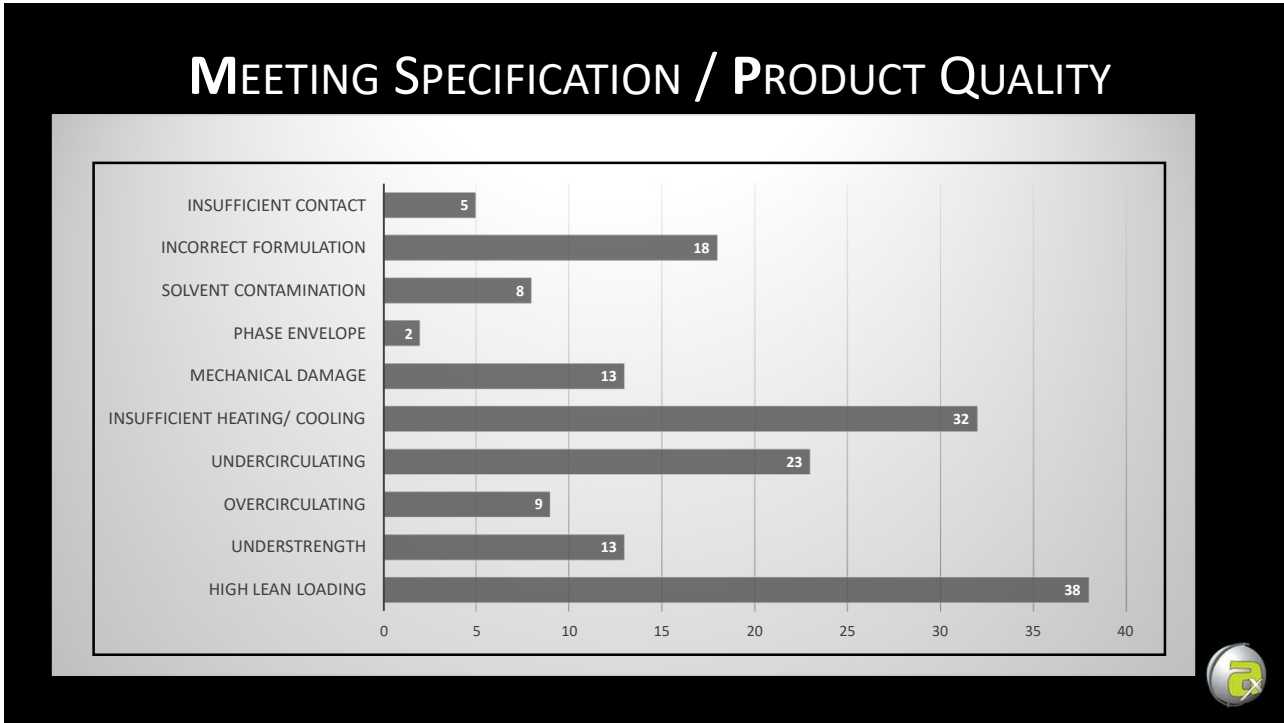


MEETING CO<sub>2</sub> SPECIFICATION

<2 MOL%  
<50 PPM (LNG)

- Primary or secondary amines provide little selectivity (DIPA is an exception)
  - Expected outlet CO<sub>2</sub> will be in ppm range
- Tertiary and hindered amines allow for the ability to custom treat CO<sub>2</sub> content
  - CO<sub>2</sub> slip can result in increased sales gas
  - provides a better feed to the SRU
  - CO<sub>2</sub> absorption is *kinetically limited* and *liquid-phase dependent*

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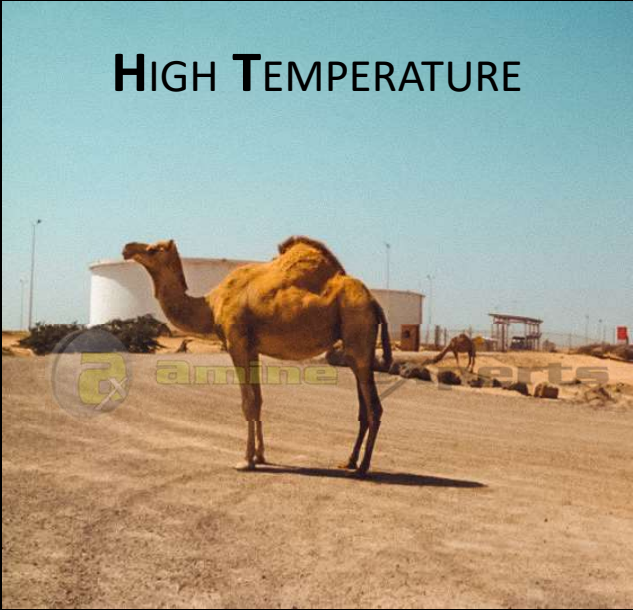




MECHANICAL DAMAGE

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# HIGH TEMPERATURE



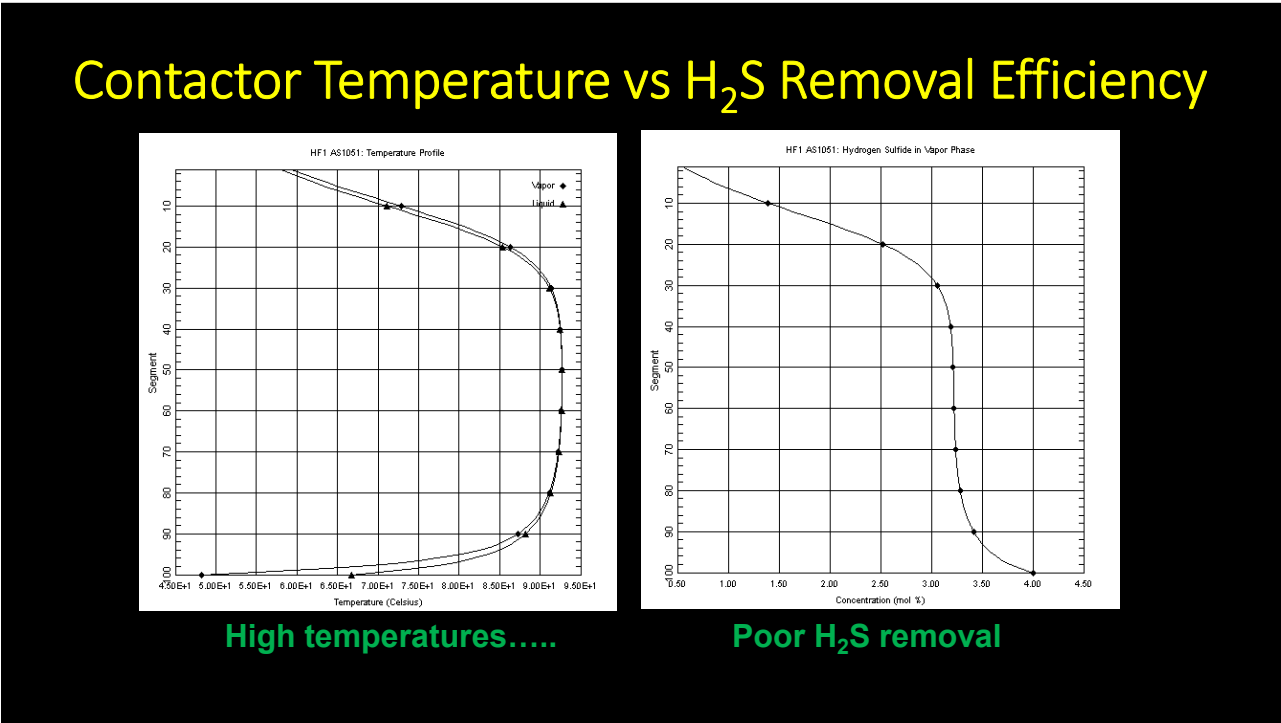
Amine solvent capacity for  $H_2S/CO_2$  absorption decreases with increasing temperature

With ambient temperatures above  $45^{\circ}C$  aerial coolers are unable to adequately cool the amine

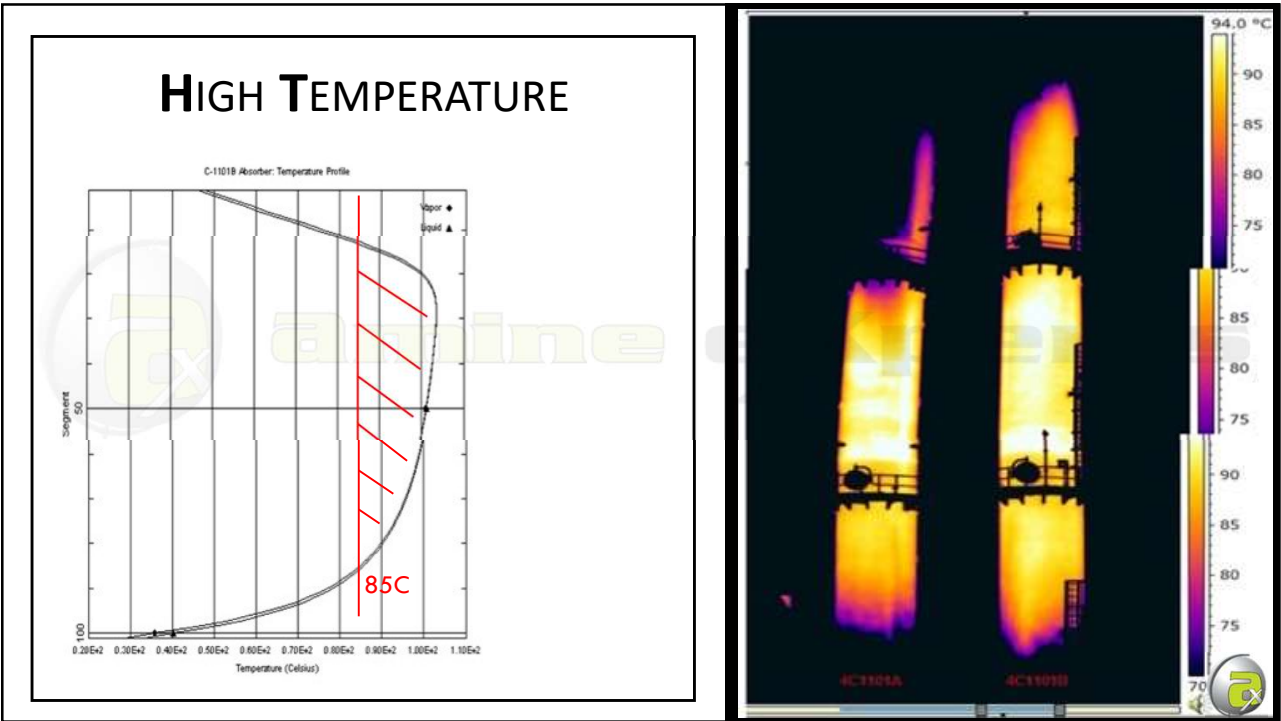
Amine temperature must be above the gas dew point.

Absorber temperature needs to be appropriate: not too hot, not too cold

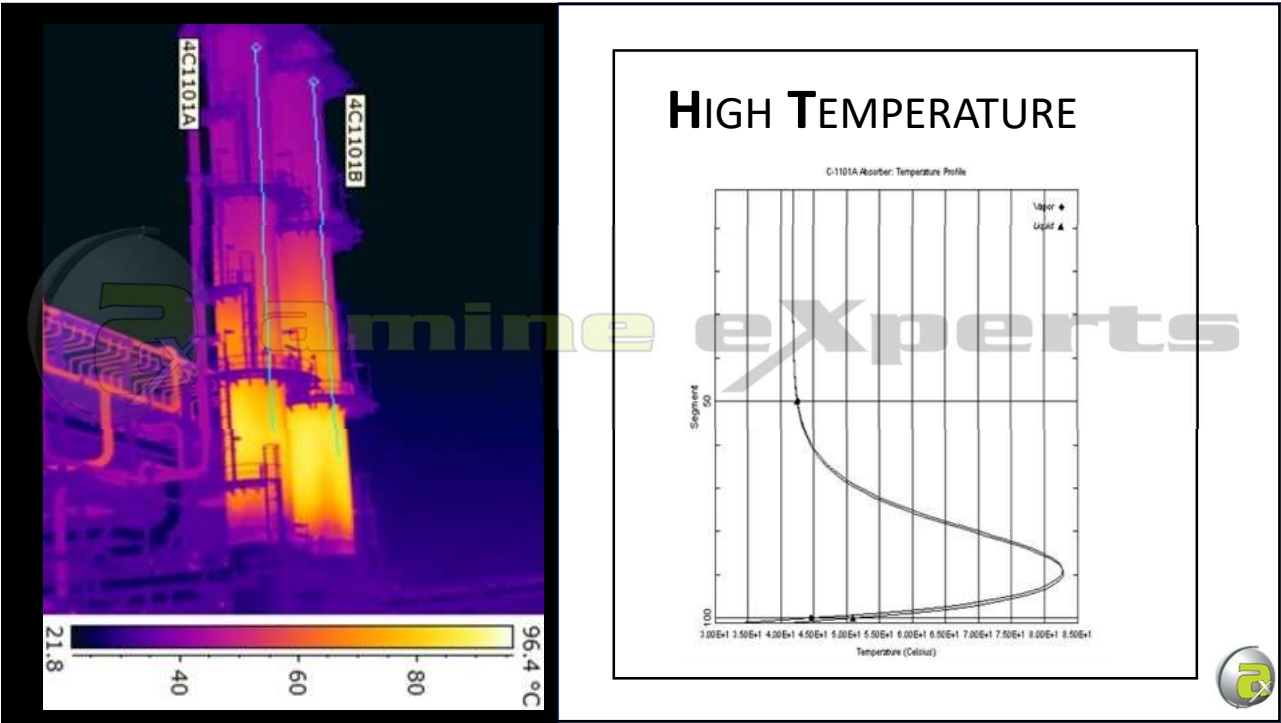
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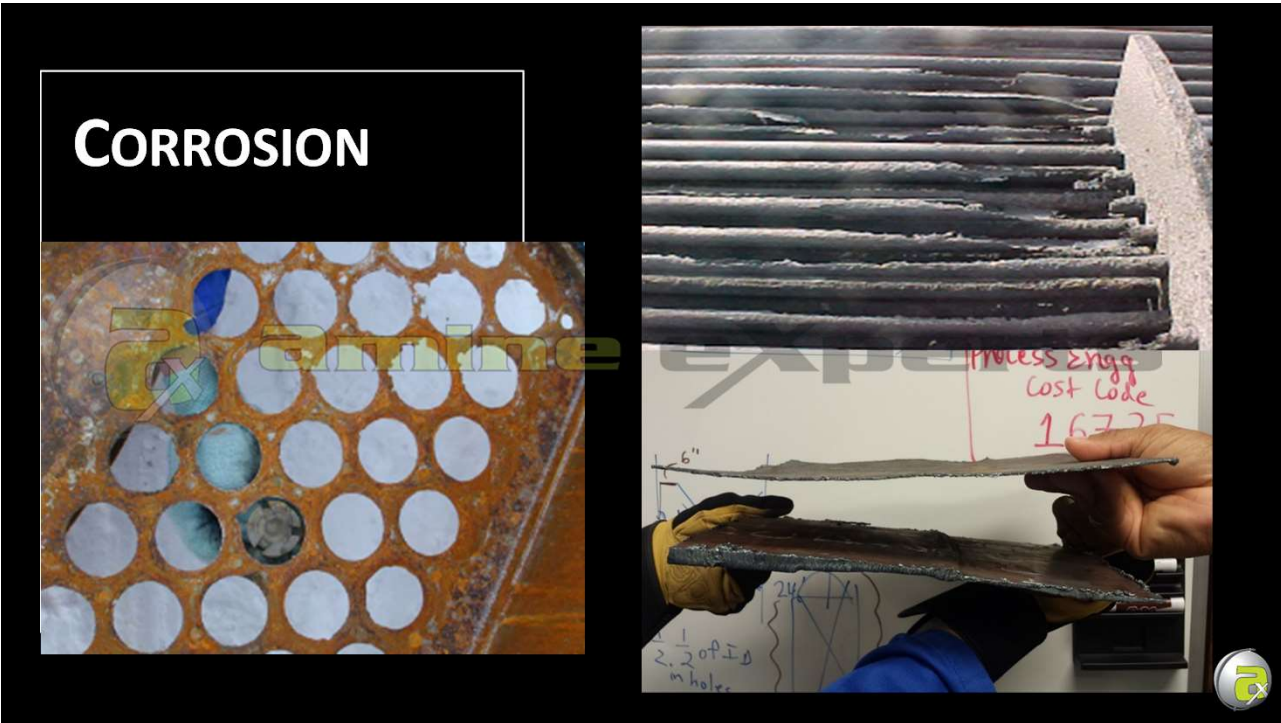
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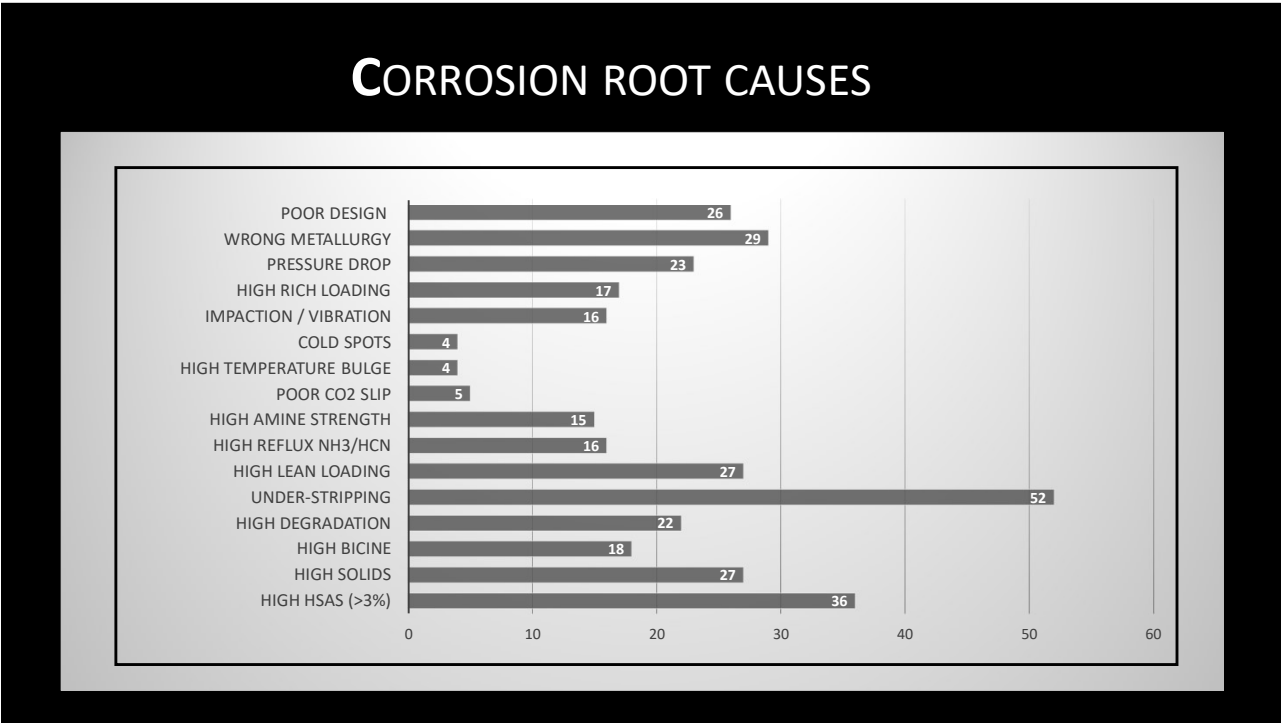
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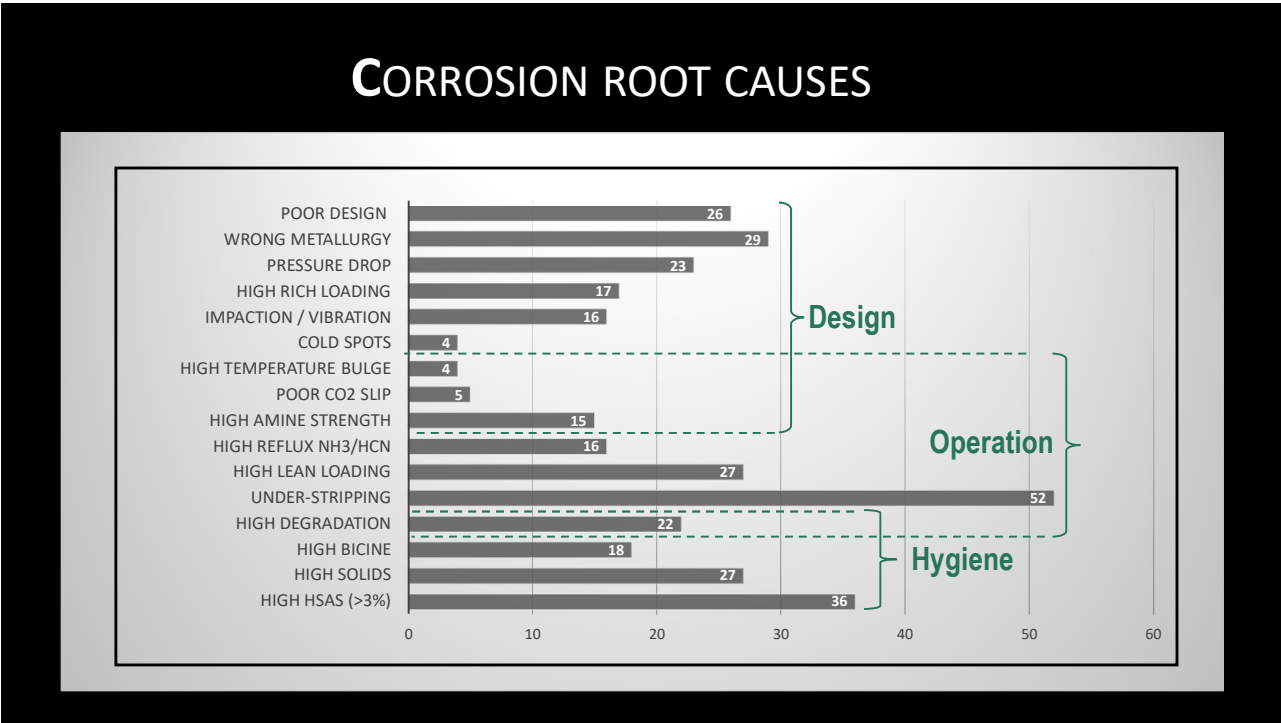
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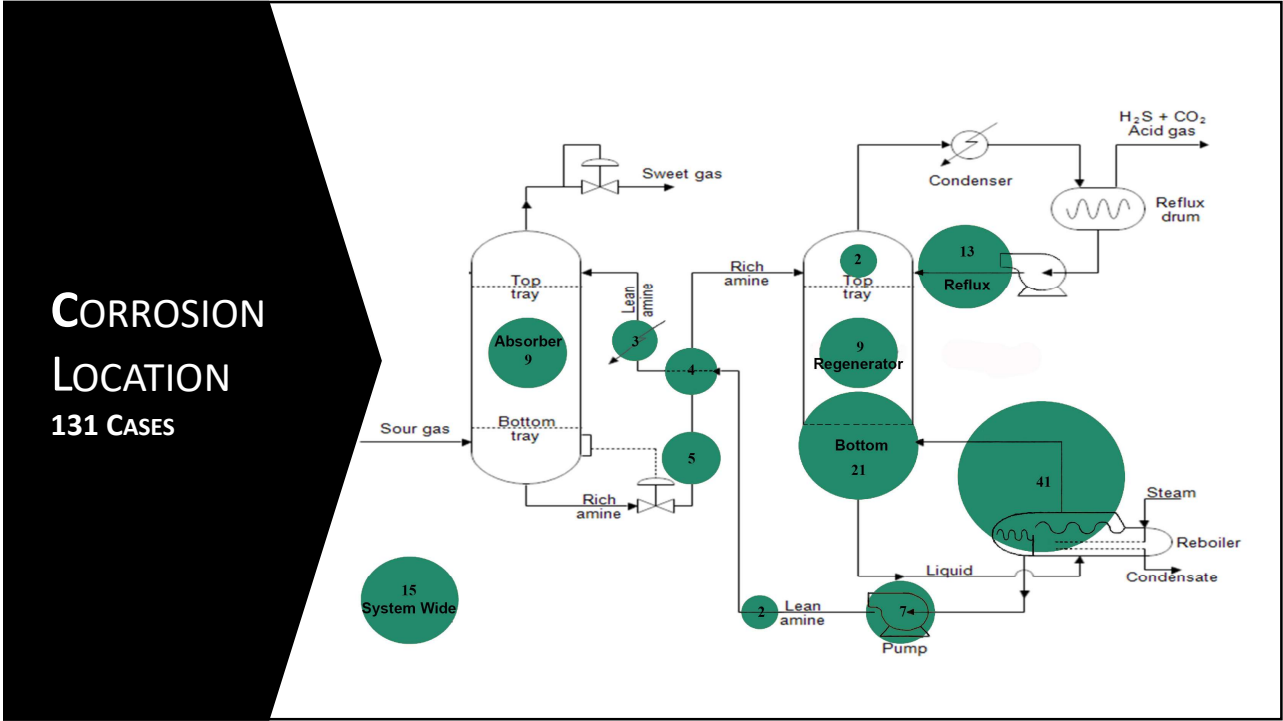
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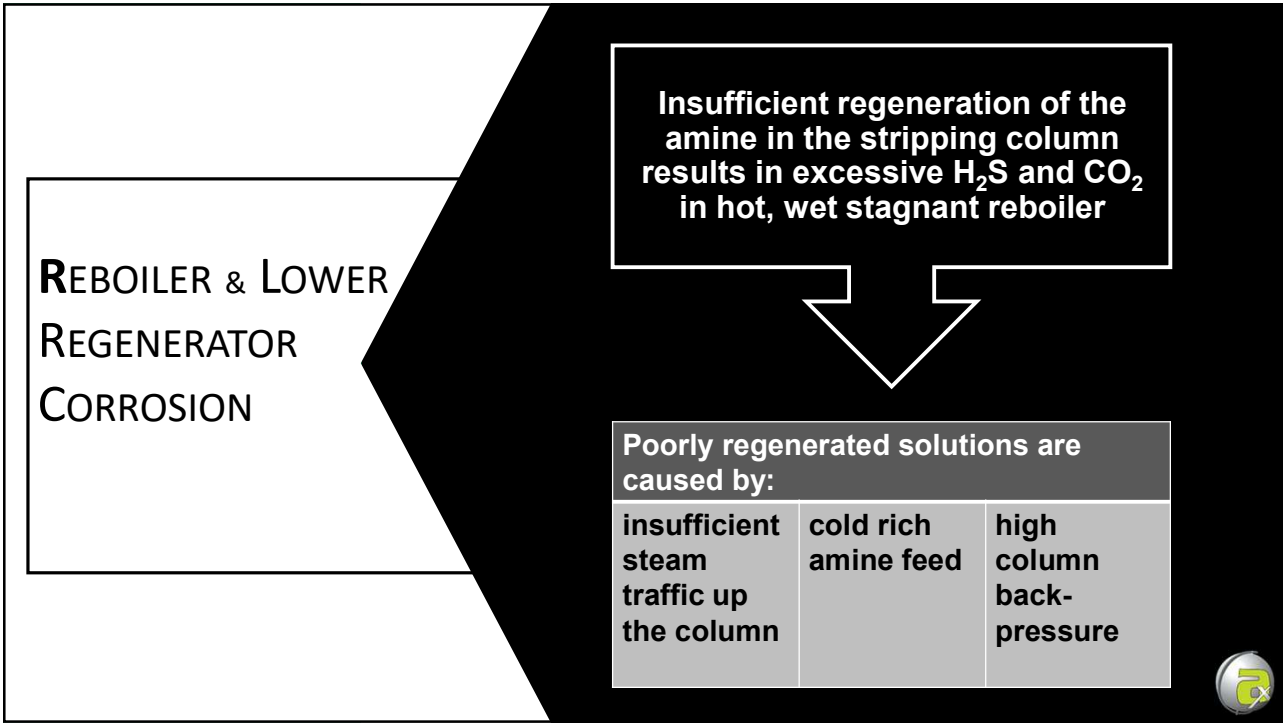
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## AMINE HYGIENE GUIDELINES

### Heat Stable Amine Salts

- Corrosion typically occurs above 3 wt% HSAS
- Exception: In conjunction with other corrosive factors corrosion in the 1.5 to 3 wt% HSAS range has been observed on some MDEA plants

### Degradation Products

- Corrosion typically occurs above 5 wt% of degradation products in the Amine Solution

*Based on Database*

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## LOADINGS & VELOCITIES

### Carbon Steel

- Rich Amine Less than 0.40 → 0.55 mol/mol
- Lean Amine less than 0.1 m/m (MEA); <0.04 m/m (DEA); <0.01 m/m (MDEA)
- Velocity less than 3 m/s

### Stainless Steel

- Rich Amine loading maximum undetermined.
- Velocity less than 6 m/s

*Based on Industry Guidelines*

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## POST WELD HEAT TREATMENT

Hydrogen diffusion into  
steel can induce cracking

Traditionally extremely  
prevalent in gas treating

Carbon steel in amine  
service **MUST** be heat  
treated




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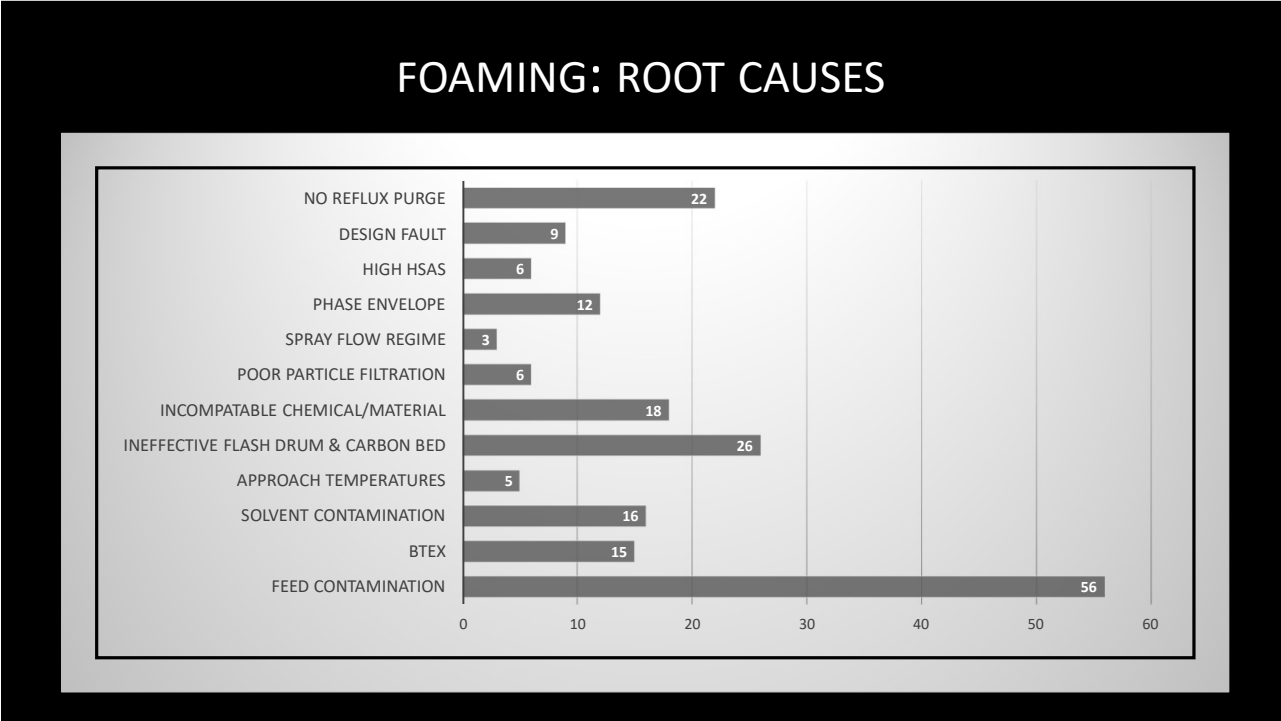
**FOAMING**



Water  
Triethanolamine  
Iso-butane  
Propane  
n-Butane  
Stearic (organic) Acid  
**Laureth 23**  
**Sodium Lauryl Sulphate**  
**Fragrance**  
**BHT**



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CONTAMINANTS IN GAS STREAMS

Liquids

- Compressor lube oils
- Hydrocarbon condensates
- Organic acids
- Pipeline Chemicals
- Completion fluids
- Well brines

Solids

- Iron sulphides
- Iron oxides
- Corrosion products
- Scale
- Dirt (silica, etc.)
- Desiccant fines
- Catalyst fines

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INLET SEPARATION

The diagram illustrates a three-stage inlet separation process. It begins with an 'INLET GAS' stream entering an 'INLET SEPARATOR'. The output from this separator is connected via a 'TIE-IN' to an 'F-500 INLET FILTER SEPARATOR'. The output from the filter separator then enters an 'INLET GAS COALESCER'. The final output from the coalescer is directed 'TO ETPD 3000 FLASH'. The diagram also shows various instrumentation points, including level indicators (LI) and pressure indicators (PFI) at different stages of the process.

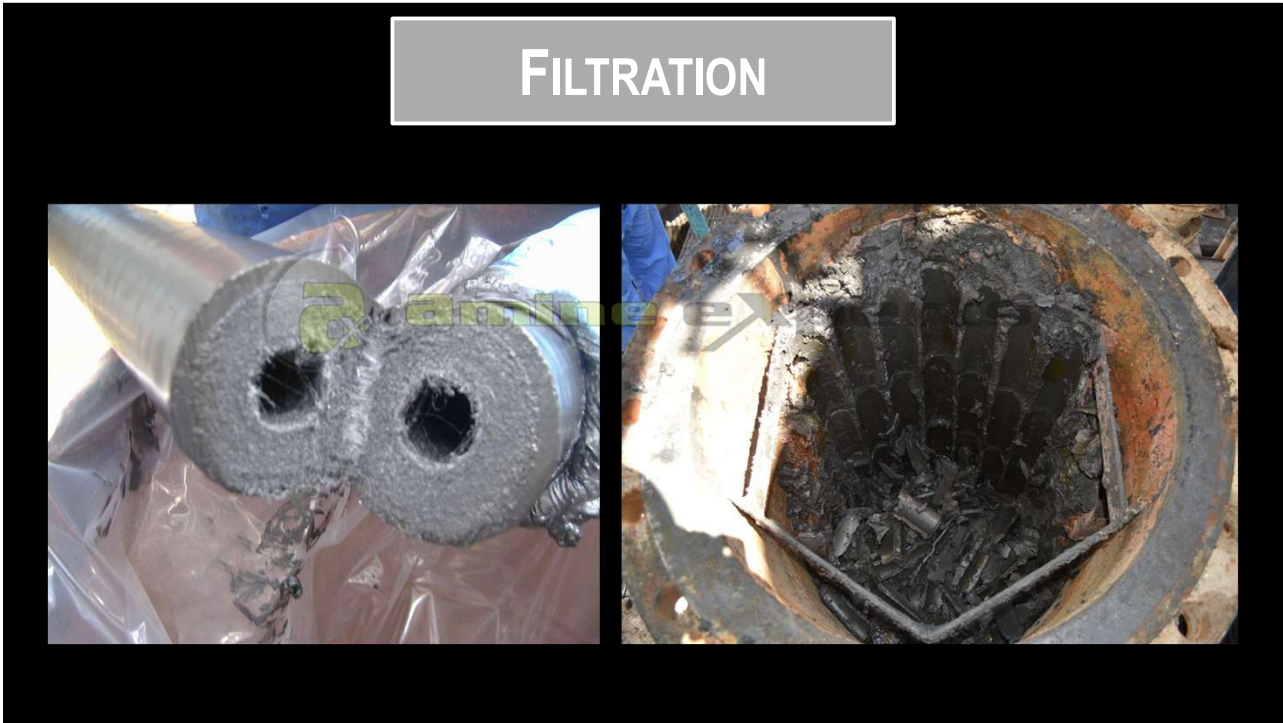
- Knock-Out Drum / 3-phase separator
- Coalescer
- Tie-Ins for:
  - Water Washes
  - Mechanical Filter

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FOAMING PLANT

A photograph showing a person holding a graduated cylinder filled with a white, frothy liquid, demonstrating foaming. The background shows a wooden structure and a gravel area. A watermark for 'amine experts' is visible in the center of the image.

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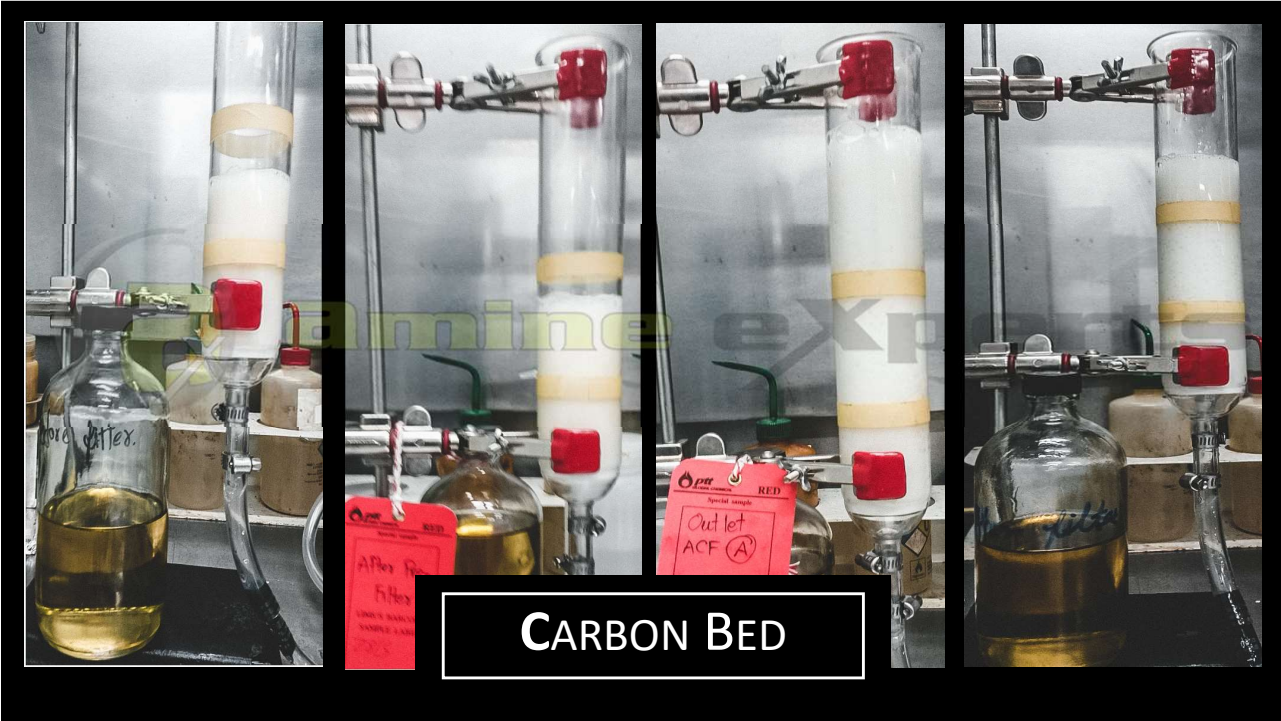


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**REFLUX PURGE:**

CONTAMINANTS CAN  
CONCENTRATE IN THE  
REFLUX LOOP



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## ANTI-FOAMING: PREVENTION OR CURE?

Anti-foam normally dramatically reduces the foaming in a system.

Continuous anti-foam dosing is generally not good practice and allows contaminants to accumulate to high levels.

Antifoams may degrade with time; antifoam injection equipment should be cleaned annually.

Anti-foams float on an aqueous surface; this means that they should not be diluted with water in an injection tote and should be injected close to the source of foaming as they do not disperse through the system

Overdosing of antifoam has been reported to result in incidents of foaming and fouling.



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## ANTI-FOAM:

SILICONE  
POLYGLYCOLS  
HIGH MW ALCOHOLS  
HIGH MW  
POLYALKYLOXALATES




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**KEY FOCUS AREAS**

<b>1.</b> LOW LEAN LOADINGS & TEMP	<b>2.</b> SEPARATION EQUIPMENT	<b>3.</b> DO NOT UNDER-STRIP THE AMINE	<b>4.</b> GOOD AMINE SYSTEM HYGIENE
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**FOCUS ON THESE AREAS WILL HALVE THE LIKELIHOOD  
OF A MAJOR SYSTEM FAILURE ON YOUR PLANT!**



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Paper available: “Trends in Tragedy –  
An In-Depth Study of Amine System Failures”

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Sulphur Experts YouTube Channel

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